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# Repetitively pulsed plasma remediation of $NO_x$ in soot laden exhaust using dielectric barrier discharges

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### Abstract

The removal of  $NO_x$  from diesel exhausts is being investigated using a variety of repetitively pulsed plasma sources. Soot particles influence  $NO_x$ densities in the gas phase of these devices through heterogeneous reactions on the soot surface. In repetitively pulsed devices, such as dielectric barrier discharges, the starting gas composition of any given pulse depends on the homogeneous and heterogeneous chemistry occurring during previous pulses. In this regard, we have computationally investigated the consequences of repetitive discharge pulses and heterogeneous chemistry on remediation of  $NO_r$  and soot oxidation. In the absence of soot, a series of discharge pulses results in increased conversion of NO to NO<sub>2</sub> compared to depositing the same energy in a single discharge pulse. With soot, single pulses result in an initial gas phase oxidation of NO to NO<sub>2</sub>, followed by heterogeneous conversion of NO<sub>2</sub> to NO on the soot. With multiple pulses and soot, due to the larger gas phase density of NO<sub>2</sub>, there is an increased flux of NO2 to the soot surface, resulting in increased soot oxidation and larger rates of heterogeneous conversion of NO<sub>2</sub> to NO. With both single and multiple discharge pulse formats, the proportion of  $NO_x$  removed, both in the presence and absence of soot, is about the same. The composition of the  $NO_x$  depends on the soot. With  $10^7 \text{ cm}^{-3}$  of 40 nm soot particles, the final NO<sub>x</sub> was primarily NO<sub>2</sub>, whereas, with  $10^9 \text{ cm}^{-3}$  of 200 nm soot particles, the  $NO_x$  was mainly NO.

### 1. Introduction

Plasma remediation is being investigated for the removal of nitrogen oxides (nitric oxide (NO) and nitrogen dioxide (NO<sub>2</sub>), together referred to as NO<sub>x</sub>) from automotive exhausts and diesel emissions in particular [1–7]. Incomplete burning of fuel and high temperatures during combustion (for higher fuel efficiency) result in unburnt hydrocarbons (UHCs) and soot particles in these exhausts. In the presence of UHCs, plasma remediation of NO primarily results in the oxidation of NO to NO<sub>2</sub> [2, 8, 9]. Catalytic converters downstream of the

plasma reactor have been investigated for reducing the plasma generated NO<sub>2</sub> to N<sub>2</sub> and O<sub>2</sub> [9–11]. Soot particles play a significant role in tropospheric NO<sub>x</sub> chemistry [12] and hence have been investigated to determine their effects on the plasma remediation of NO<sub>x</sub> [13, 14].

A number of experimental and modelling investigations have addressed the discharge phenomena and reaction kinetics during the plasma remediation NO<sub>x</sub> using dielectric barrier discharges (DBDs) [1, 2, 6, 15–17]. Due to the uncertainty in composition of diesel exhausts resulting from the inherent variation in the composition of diesel fuels, model gases are often used as surrogates. A typical model gas composition is N<sub>2</sub>/O<sub>2</sub>/H<sub>2</sub>O/CO<sub>2</sub> = 79/8/6/7 with hundreds of parts

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per million (ppm) of NO, CO, H<sub>2</sub> and UHCs. N<sub>2</sub> and O<sub>2</sub> are from the excess air used for combustion whereas H<sub>2</sub>O and CO2 are products of combustion. Investigations using ethene  $(C_2H_4)$  [2] as a model UHC showed that for an energy deposition of  $25 \text{ J} \text{ I}^{-1}$  the W-value (energy required to remove one molecule) for NO improved from 60 eV without ethene to 10 eV with 2000 ppmv of C<sub>2</sub>H<sub>4</sub>. Although 100% NO removal was achieved, most of it was converted to NO<sub>2</sub>. Using propene  $(C_3H_6)$  and propane  $(C_3H_8)$  [8] as model UHCs, the NO<sub>x</sub> removal at 56 J1<sup>-1</sup> increased from 12% without propene to 32% with 175 ppm C<sub>3</sub>H<sub>6</sub>. The primary products were HNO<sub>3</sub>, HNO<sub>2</sub>, organic nitrates and nitrites. In experimental studies with 100 ppm  $C_3H_6$  and 500 ppm NO in a  $N_2/O_2 = 90/10$ mixture at 300°C, Penetrante et al [9] observed nearly 100% NO removal at  $50 \text{ J} \text{ I}^{-1}$ . Without C<sub>3</sub>H<sub>6</sub>, less than 10% of the NO was removed. Experiments on plasma soot oxidation performed by Thomas et al [13] using real diesel exhausts showed that as high as  $1.2 \,\mathrm{J}\,\mu\mathrm{g}^{-1}$  might be required for the removal of soot particles. In studies on soot removal by Müller et al [18, 19], a DBD reactor coupled with a particle filter (to increase the residence time of soot particles) was used to decompose soot particles in real diesel exhausts. More than 95% of the soot was removed, with the primary decomposition

of soot to CO occurred mainly in the presence of  $NO_2$ , demonstrating the importance of  $NO_2$  in the mechanism for soot oxidation. In all of the above studies, the primary NO remediation product was  $NO_2$  and so there was little change in the net

product was NO<sub>2</sub> and so there was little change in the net NO<sub>x</sub>. However, plasma remediation is still considered a viable technology since there are efficient catalytic converters for the subsequent remediation of NO<sub>2</sub>. For example, Balmer *et al* [11] observed as high as 70% NO<sub>x</sub> remediation at 50 J1<sup>-1</sup> in simulated exhausts when using a plasma reactor coupled with a proprietary catalyst. When the plasma reactor alone was used, the NO<sub>x</sub> removal was less than 20%. In a strict sense, only the conversion of NO to N<sub>2</sub> should be considered as remediation as the products of NO<sub>x</sub> remediation such as HNO<sub>2</sub>, HNO<sub>3</sub>, organic nitrates and nitrites, when released to the atmosphere, can photolytically degrade to regenerate NO and NO<sub>2</sub> [20]. Nevertheless, when we refer to remediation or removal here, it is only for the conversion of NO<sub>x</sub> to other compounds.

products being CO and CO<sub>2</sub>. They observed that the oxidation

In an earlier investigation, we showed that  $NO_x$  removal increased by nearly 10% in the presence of 100 nm diameter soot particles having a density of  $10^8 \text{ cm}^{-3}$  [14]. We also showed that repetitively pulsed discharges are more efficient for  $NO_x$  remediation compared to depositing the same energy in a single pulse [21]. For example, the *W*-value for  $NO_x$ remediation decreased from 240 eV for a single pulse (58 J1<sup>-1</sup>) to 185 eV when the same energy was distributed over 20 pulses. The interaction of products of previous pulses with the species during the current pulse allowed for a different chemistry in the repetitively pulsed case which ultimately improved remediation.

In this paper, we report on a computational investigation of the combined effects of repetitive discharge pulses and soot on  $NO_x$  remediation and soot oxidation. Using a pseudohomogeneous global kinetics model, the consequences of varying energy deposition, inlet UHC concentration, soot diameter, and soot particle number density on  $NO_x$  remediation and soot oxidation are parametrized for cases when using a single discharge pulse and when using multiple pulses. We found that, for a given energy deposition,  $NO_x$  remediation improved when using multiple pulses in the presence of soot compared to single pulse processing with or without soot, or repetitive pulse processing without soot. Due to there being larger NO<sub>2</sub> densities when using multiple pulses, there is also more soot oxidation. With single pulses, the exit composition of NO<sub>x</sub> was primarily NO, whereas when using multiple pulses, the exit composition of  $NO_{x}$  was mainly  $NO_{2}$ . The soot particle number density and diameter significantly influence the exit composition of  $NO_x$  but have a negligible effect on the total  $NO_x$  density. The model used for this study, GLOBAL\_KIN, is described in section 2. Results for repetitively pulsed plasma processing of  $NO_x$  and oxidation of soot are discussed in section 3. Concluding remarks are in section 4

# 2. Description of the model

The model used for this investigation has been previously described in detail [14] and hence will only be briefly described here. GLOBAL\_KIN is a homogeneous gas phase plasma chemistry simulator. The model DBD plasma reactor is analogous to a well-mixed batch or plug flow system sustained between two dielectric slabs backed by metal plates. Typically, tens of kilovolts across the electrodes are required to produce a discharge in the exhaust contained in a gap of a few millimetres.

To account for reactions at the soot surface and transport of gas phase species to the soot, a quasi-homogeneous gas phase model is used (see figure 1). With soot particles having diameter  $d_s$ , species in bulk plasma diffuse to the soot surface through a boundary layer of thickness  $\delta$ . The algorithms for species transport and heterogeneous chemistry on the soot surface, discussed in detail in [14], take advantage of the fact that the boundary layer thickness is approximately equal to the radius of the soot particle for typical plasma processing conditions.



**Figure 1.** Quasi-homogeneous model for soot oxidation. The region surrounding the soot particle of diameter  $d_s$  is divided into two zones: a homogeneous bulk plasma region and a diffusion boundary layer having thickness  $\delta$ . Species in the bulk plasma diffuse through the boundary layer to react at the soot surface. Desorbed products from the soot diffuse back into the bulk plasma thereby modifying the bulk composition. The soot is composed of spherules having diameter  $d_{sp}$  and has an overall fractal dimension of 2.8. For the conditions typical of diesel exhausts,  $d_s = 100$  nm,  $\delta = 50$  nm,  $d_{sp} = 20$  nm.

Ordinary differential equations (ODEs) for the time rate of change of gas phase and soot-surface species densities are constructed based on a user-defined reaction mechanism. Electron impact reaction rate coefficients are obtained by solving Boltzmann's equation for the electron energy distribution using a two-term spherical harmonic expansion [22]. The resulting reaction rate constants are then tabulated as a function of average electron energy and interpolated during the execution of the model. The ODEs for species densities and circuit parameters are then integrated in time using a variable coefficient ODE solver [23].

The soot modelled in this study is composed of carbon and hydrogen. The soot specific surface area was determined based on experiments reporting that the particles are composed of approximately 20 nm spherules having a fractal structure [24]. A fractal dimension of 2.8 was used [25]. Further details on the soot structure and properties are in [14].

The reaction set used in this study includes electron impact reactions with the background gases producing ions, electrons, and free radicals; gas phase heavy particle reactions; and reactions of gas phase species with the soot. The reaction mechanism contained 88 gas phase species and 350 reactions. Since the gas phase reaction mechanism for NO<sub>x</sub> remediation with UHCs has been discussed previously [21], only those reactions particularly germane to this study will be addressed.

Adsorption kinetics on the soot surface are described by a sticking probability  $\gamma_i$ , which depends on the surface coverage. Employing a standard surface site balance model,  $\gamma_i = \gamma_{i-0}\theta/\theta_0$ , where  $\gamma_{i-0}$  is the sticking probability for species *i* when all adsorption sites are empty,  $\theta$  is the number of sites available for adsorption and  $\theta_0$  is the total site density. We used  $\theta_0 = 10^{15}$  cm<sup>-2</sup>, similar to that reported for the adsorption sites for NO<sub>2</sub> on soot [26]. The adsorption probabilities of NO<sub>2</sub>, O and OH used in this study are in table 1. Due to uncertainties in the reaction probabilities of NO<sub>2</sub>, we previously performed parametrizations to quantify the sensitivity of NO<sub>x</sub> remediation to these parameters [14]. Varying  $\gamma_0$ (NO<sub>2</sub>) from 10<sup>-4</sup> to 10<sup>-1</sup> resulted in large changes in NO densities (nearly 100% increase with this increase in  $\gamma_0$ (NO<sub>2</sub>)) while the NO<sub>x</sub> density remained almost a constant. For this study,  $\gamma_0$ (NO<sub>2</sub>) = 0.1 [30].

The rate constant for NO<sub>2</sub> desorption from soot was  $10^3 \text{ s}^{-1}$  [26], a value reported for a soot temperature of 300 K. At higher temperatures, as is our case, desorption is likely to occur at higher frequencies and hence, this value serves as a lower limit. Although O and OH adsorption on soot are included for completeness, their contribution to the overall soot oxidation under normal operating conditions is less than 1%. More than 99% of the soot oxidation occurs by reaction with NO<sub>2</sub> [14]. This is due to the higher frequencies for gas phase consumption of O and OH compared to their heterogeneous consumption.

Table 1. Reaction probabilities at soot surface.

Species	Reaction probability	References
NO <sub>2</sub>	0.10	[27]
0	0.10	[28]
OH	0.12	[29]

The base case operating conditions are 1 atm, 453 K, gas residence time of 0.2 s (space velocity of  $18000 \,h^{-1}$ ) and an electrode spacing of 0.25 cm. The gas mixture is  $N_2/O_2/H_2O/CO_2 = 79/8/6/7$  with 260 ppm NO, 400 ppm CO, 133 ppm H<sub>2</sub>, and 500 ppm  $C_3H_6$ . The soot density and diameter are  $10^8 \text{ cm}^{-3}$  and 100 nm. The energy deposition is  $30 \text{ J}1^{-1}$  (10% fuel economy for a diesel engine [31]) which, for a single pulse, corresponds to a discharge voltage of 18 kV. To address repetitively pulsed discharges, 100 Hz here, the model is executed for a series of current pulses and afterglow periods (20 for the 0.2 s residence time). The initial conditions for a discharge pulse are given by the species densities at the end of the previous afterglow. To achieve the same energy deposition with repetitive pulses, the applied voltage is 13 kV. Although there are differences in excitation rates resulting from the different voltages, these differences do not prejudice any comparisons. When varying energy deposition, either the voltage or the permittivity of the dielectric was changed.

Electron density  $(n_e)$  and temperature  $(T_e)$  are shown in figure 2 for the base case conditions when using single and multiple pulses. The current pulse lasts approximately 145 ns for a single pulse and approximately 165 ns for multiple pulses. The longer current pulse when using repetitive pulses is due to the slower avalanche resulting from the lower applied voltage. Electrons, accelerated by the electric field, collide with the background gases producing positive ions and secondary electrons, dominantly by,

$$\mathbf{e} + \mathbf{N}_2 \to \mathbf{N}_2^+ + \mathbf{e} + \mathbf{e},\tag{1}$$

$$\mathbf{e} + \mathbf{O}_2 \to \mathbf{O}_2^+ + \mathbf{e} + \mathbf{e},\tag{2}$$

$$e + H_2O \rightarrow H_2O^+ + e + e, \qquad (3)$$

$$e + CO_2 \rightarrow CO_2^+ + e + e. \tag{4}$$

For a single discharge pulse, the peak electron density is  $\approx 10^{13} \text{ cm}^{-3}$  and the peak electron temperature is  $\approx 3 \text{ eV}$ . With repetitive pulses, less energy is deposited per pulse and, as a result, the peak electron density is  $\approx 0.03 \times 10^{13} \text{ cm}^{-3}$ , while the peak electron temperature is  $\approx 3 \text{ eV}$ . Since the current pulse is wider (165 ns) with repetitive pulses than with a single pulse (145 ns) the peak  $n_e$  at high pulse repetition frequency (PRF) is less than 1/20 of the single pulse value. The time dependences of  $n_e$  and  $T_e$  for the first and last pulse of the repetitive pulse case do not differ appreciably because the mole fractions of the major background gases do not change significantly.

Although the chemistry of interest is dominantly through free-radical reactions, it is nevertheless instructive to also discuss the ion chemistry. Since the ion chemistry does not significantly differ between single and repetitive pulses due to the shorter timescales for ion reactions (hundreds of nanoseconds), we will discuss the ion chemistry for single pulses.

The initiating reactions for ion chemistry are electron impact ionizations producing  $N_2^+$ ,  $O_2^+$ ,  $H_2O^+$  and  $CO_2^+$ 



**Figure 2.** Plasma parameters for single and repetitive pulses: (*a*)  $n_e$ ,  $T_e$  for a single pulse; (*b*)  $n_e$ ,  $T_e$  during the first pulse of 20 pulses; (*c*)  $n_e$ ,  $T_e$  for the last pulse of 20 pulses. Conditions are 1 atm, 453 K, N<sub>2</sub>/O<sub>2</sub>/H<sub>2</sub>O/CO<sub>2</sub> = 79/8/6/7 with 260 ppm NO, 400 ppm CO, 133 ppm H<sub>2</sub>, and 500 ppm C<sub>3</sub>H<sub>6</sub>. Gas residence time is 0.2 s and the gas gap is 2.5 mm. The applied voltage for the single pulse case is 18 kV and that for 20 pulses is 13 kV for total energy deposition of  $30 \text{ J1}^{-1}$ . Following the current pulse (around 150 ns), electrons are lost primarily by attachment to H<sub>2</sub>O and O<sub>2</sub>.

(equations (1)–(4)). Nearly 46% of the  $N_2^+$  formed undergoes charge exchange reactions with  $H_2O$  to form  $H_2O^+$ ,

$$N_{2}^{+} + H_{2}O \rightarrow H_{2}O^{+} + N_{2}$$
  

$$k = 2.0 \times 10^{-9} \text{ cm}^{3} \text{ s}^{-1} [32], \qquad (5)$$

where *k* is the rate coefficient for the reaction. Most of the remaining  $N_2^+$  (52%) dimerizes with  $N_2$  to form  $N_4^+$  which then charge exchanges with  $O_2$  to form  $O_2^+$ ,

$$N_{2}^{+} + N_{2} + M \to N_{4}^{+} + M$$
  

$$k = 1.1 \times 10^{-29} \,\mathrm{cm}^{6} \,\mathrm{s}^{-1} \ [33], \qquad (6)$$

$$N_{4}^{+} + O_{2} \rightarrow O_{2}^{+} + N_{2} + N_{2}$$
  

$$k = 2.5 \times 10^{-10} \,\mathrm{cm}^{3} \,\mathrm{s}^{-1} \,\,[33].$$
(7)

 $O_2^+$  is also formed by charge exchange reactions of  $H_2O^+$  and  $CO_2^+$  with  $O_2$ ,

$$H_2O^+ + O_2 \to O_2^+ + H_2O$$
  

$$k = 4.3 \times 10^{-10} \text{ cm}^3 \text{ s}^{-1} [33], \qquad (8)$$

$$CO_{2}^{+} + O_{2} \rightarrow O_{2}^{+} + CO_{2}$$
  

$$k = 5.6 \times 10^{-11} \text{ cm}^{3} \text{ s}^{-1} [33].$$
(9)

About 66% of the  $CO_2^+$  is consumed by the above reaction. The remainder is lost by charge neutralization reactions with  $O^-$  and  $H^-$ .

Almost all of the  $O_2^+$  formed by the above reactions associates with  $H_2O$  to form  $O_2^+ \cdot H_2O$ , which further reacts with  $H_2O$  to form  $H_3O^+$ ,

$$O_{2}^{+} + H_{2}O + M \rightarrow O_{2}^{+} \cdot H_{2}O + M$$
  

$$k = 2.5 \times 10^{-28} \,\mathrm{cm}^{6} \,\mathrm{s}^{-1} \ [33], \qquad (10)$$

$$O_{2}^{+} \cdot H_{2}O + H_{2}O \rightarrow H_{3}O^{+} + OH + O_{2}$$
  

$$k = 1.2 \times 10^{-9} \text{ cm}^{3} \text{ s}^{-1} [33].$$
(11)

 $H_3O^+$  is also formed from  $H_2O^+$ ,

$$H_2O^+ + H_2O \to H_3O^+ + OH$$
  

$$k = 1.7 \times 10^{-9} \text{ cm}^3 \text{ s}^{-1} [33].$$
(12)

 $H_3O^+$  reacts with  $H_2O$  to form the complex ion,  $H_3O^+ \cdot H_2O$ ,

$$H_{3}O^{+} + H_{2}O + M \to H_{3}O^{+} \cdot H_{2}O + M$$
  

$$k = 5.0 \times 10^{-27} \text{ cm}^{6} \text{ s}^{-1} [33].$$
(13)

Electrons are dominantly lost by dissociative attachment to  $H_2O(73\%)$ ,  $CO_2(3\%)$  and  $O_2(24\%)$  (both dissociative and non-dissociative),

$$e + H_2 O \to H^- + OH, \tag{14}$$

$$e + CO_2 \to O^- + CO, \tag{15}$$

$$\mathbf{e} + \mathbf{O}_2 \to \mathbf{O}^- + \mathbf{O},\tag{16}$$

$$e + O_2 + M \to O_2^- + M.$$
 (17)

The densities of  $H_3O^+ \cdot H_2O$ ,  $N_4^+$ ,  $O^-$  and  $H^-$  as a function of time are shown in figure 3. The rapid decay of  $N_4^+$  is by reaction with  $O_2$  forming  $O_2^+$  (equation (7)).  $O^-$  and  $H^$ neutralize less rapidly by collisions with  $H_3O^+ \cdot H_2O$  to produce  $H_2O$ , OH and  $H_2$ ,

$$H_{3}O^{+} \cdot H_{2}O + O^{-} \to H_{2}O + H_{2}O + OH$$
  

$$k = 3.0 \times 10^{-6} \text{ cm}^{3} \text{ s}^{-1} [33], \qquad (18)$$

$$H_{3}O^{+} \cdot H_{2}O + H^{-} \rightarrow H_{2}O + H_{2}O + H_{2}$$
  
$$k = 3.0 \times 10^{-6} \text{ cm}^{3} \text{ s}^{-1} [33].$$
(19)

The free-radical reactions are initiated by the electron impact dissociation of the background gases producing N, O, OH and H,

$$e + N_2 \rightarrow N + N + e, \qquad (20)$$

$$\mathbf{e} + \mathbf{O}_2 \to \mathbf{O} + \mathbf{O} + \mathbf{e},\tag{21}$$

$$e + H_2O \rightarrow OH + H + e, \qquad (22)$$

$$e + CO_2 \rightarrow O + CO + e. \tag{23}$$

The densities of N, O, OH and H as a function of time are shown in figure 4 for a single pulse, and for the first and the



**Figure 3.** Time dependence of the densities of charged species during the single pulse plasma processing of  $NO_x$ . The dominant positive ion is  $H_3O^+ \cdot H_2O$  and the dominant negative ions are  $O^-$  and  $H^-$ , which are primarily lost by charge neutralizations with each other. The conditions are the same as for figure 2.



**Figure 4.** Time dependence of N, O, OH and H densities: (*a*) single pulse; (*b*) first of 20 repetitive pulses; (*c*) 20th of 20 pulses. Conditions are same as for figure 2. Electron impact reactions with  $N_2$ ,  $O_2$ ,  $H_2O$  and CO produce N, O, OH and H.

last pulse of the multiple pulse case. Recalling that the current pulse is  $\approx 150$  ns, the production of these primary radicals is dominantly from electron impact reactions. Reactions with neutral species then determine the disposition of this initial inventory of radicals. N atoms are dominantly consumed by reactions with NO, NO<sub>2</sub>, CO<sub>2</sub> and O<sub>2</sub>,

N + NO → N<sub>2</sub> + O  

$$k = 3.4 \times 10^{-11} \exp\left(-\frac{24}{T}\right) \text{ cm}^3 \text{ s}^{-1},$$

$$k_{298} = 3.2 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1} [33],$$
(24)

$$N + NO_2 \rightarrow N_2O + O$$
  
 $k = 2.4 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  [33], (25)

N + NO<sub>2</sub> → NO + NO  

$$k = 9.9 \times 10^{-13} \text{ cm}^3 \text{ s}^{-1}$$
 [33], (26)

$$N + CO_{2} \rightarrow CO + NO$$

$$k = 3.2 \times 10^{-13} \exp\left(-\frac{1710}{T}\right) \text{ cm}^{3} \text{ s}^{-1},$$

$$k_{298} = 1.0 \times 10^{-15} \text{ cm}^{3} \text{ s}^{-1} \text{ [34]},$$
(27)

N + O<sub>2</sub> → NO + O  

$$k = 4.4 \times 10^{-12} \exp\left(-\frac{3220}{T}\right) \text{ cm}^3 \text{ s}^{-1},$$

$$k_{298} = 7.7 \times 10^{-17} \text{ cm}^3 \text{ s}^{-1} [35],$$
(28)

where  $k_{298}$  is the rate constant at 298 K. When using a single pulse, the contribution to N consumption from the reactions with NO, NO<sub>2</sub>, CO<sub>2</sub> and O<sub>2</sub> (equations (24)–(28)) are 89.0%, 0.2%, 5.0% and 3.0%, respectively. With repetitive pulses, the contributions are 63.0%, 14.0%, 14.0% and 8.0%. The higher contribution from NO<sub>2</sub> for N consumption with multiple pulses is a result of an increased overlap in time of the NO<sub>2</sub> and N atom densities. The density of NO, a major consumer of N atoms, decreases during later pulses (explained below). As a result, the N atom densities are sustained for longer periods during the latter pulses compared to the first pulse when using repetitive pulses.

With repetitive pulses, the peak O density is  $\approx 10^{14}$  cm<sup>-3</sup> in any given pulse as compared with  $2 \times 10^{15}$  cm<sup>-3</sup> for a single pulse. The peak O atom densities for the first and last of 20 pulses, determined largely by electron impact, are similar because the density of O<sub>2</sub> remains nearly a constant. O atoms are primarily consumed by reactions with C<sub>3</sub>H<sub>6</sub>, NO<sub>2</sub> and O<sub>2</sub>,

O + C<sub>3</sub>H<sub>6</sub> → Methyl Oxirane  

$$k = 1.2 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$$
 [36], (29)

$$O + C_3 H_6 \to C_2 H_5 CHO$$
  

$$k = 1.2 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1} [36], \qquad (30)$$

$$O + C_3 H_6 \to CH_2 CHO + CH_3$$
  

$$k = 0.8 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1} [36], \qquad (31)$$

$$O + C_3 H_6 \to C_2 H_5 + HCO$$
  

$$k = 0.8 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1} [36], \qquad (32)$$

$$O + NO_{2} \rightarrow NO + O_{2}$$
  

$$k = 6.5 \times 10^{-12} \exp\left(\frac{120}{T}\right) \text{ cm}^{3} \text{ s}^{-1},$$
  

$$k_{298} = 9.7 \times 10^{-12} \text{ cm}^{3} \text{ s}^{-1} \text{ [35]},$$
(33)

$$O + O_2 + M \rightarrow O_3 + M$$
  
 $k = 3.4 \times 10^{-34} \exp\left(\frac{T}{298}\right)^{-1.2} \text{ cm}^6 \text{ s}^{-1} \text{ [34].}$  (34)

Using single pulses, the contributions of the reactions with  $C_3H_6$ ,  $NO_2$  and  $O_2$  (equations (29)–(34)) towards O consumption are 56%, 4% and 11%, respectively. When using repetitive pulses, the contributions are 56%, 25% and 12%. The larger contribution to O consumption by the reaction with  $NO_2$  with multiple pulses is due to the increased overlap in time of  $NO_2$  and O atom densities. The more rapid consumption of O in the first pulse is due to the higher densities of  $C_3H_6$  during the first pulse compared to the last.

OH radicals are consumed primarily by reactions with  $C_3H_6$  forming  $C_3H_6OH$  (hydroxy alkyl radicals), HCHO forming HCO, NO<sub>2</sub> forming HNO<sub>3</sub> and NO forming and HNO<sub>2</sub>,

OH + C<sub>3</sub>H<sub>6</sub> 
$$\rightarrow$$
 0.65 CH<sub>3</sub>CHCH<sub>2</sub>OH + 0.35 CH<sub>3</sub>CH(OH)CH<sub>2</sub>  
 $k = 4.9 \times 10^{-12} \exp\left(\frac{504}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k_{298} = 2.6 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1}$  [36], (35)

 $OH + HCHO \rightarrow HCO + H_2O$ 

$$k = 4.7 \times 10^{-12} \left(\frac{T}{298}\right)^{1.2} \exp\left(\frac{225}{T}\right) \text{ cm}^6 \text{ s}^{-1},$$
  

$$k_{298} = 1.0 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1} \text{ [37]},$$
(36)

OH + NO<sub>2</sub> + M 
$$\rightarrow$$
 HNO<sub>3</sub> + M  
 $k = 4.6 \times 10^{-29} \left(\frac{T}{298}\right)^{-5.5} \exp\left(-\frac{1183}{T}\right) \text{ cm}^6 \text{ s}^{-1},$   
 $k_{298} = 8.7 \times 10^{-31} \text{ cm}^6 \text{ s}^{-1}$  [38], (37)

 $OH + NO + M \rightarrow HNO_2 + M$ 

$$k = 8.6 \times 10^{-31} \left(\frac{T}{298}\right)^{-2.5} \exp\left(\frac{34}{T}\right) \,\mathrm{cm}^{6} \,\mathrm{s}^{-1},$$
  

$$k_{298} = 9.7 \times 10^{-31} \,\mathrm{cm}^{6} \,\mathrm{s}^{-1} \,\,[38]. \tag{38}$$

The contributions of reactions of  $C_3H_6$ , HCHO, NO<sub>2</sub> and NO (equations (35)–(38)) to OH consumption are 66%, 5%, 7% and 4% when using a single pulse. With multiple pulses, the contributions are 72%, 11%, 10% and 4%. OH consumption is more rapid in the last pulse compared to the first due to increased rates of reactions with HCHO and NO<sub>2</sub> which have larger densities during the last pulse.

In the absence of UHCs, the radicals primarily responsible for the oxidation of NO to NO<sub>2</sub> in the gas phase are HO<sub>2</sub> and O<sub>3</sub>. With UHCs, radicals such as CH<sub>3</sub>CH(OH)CH<sub>2</sub>OO and CH<sub>3</sub>CH(OO)CH<sub>2</sub>OH ( $\beta$ -hydroxy alkyl peroxies, in short  $\beta$ HAPs) are produced, which oxidize NO to NO<sub>2</sub>. The reaction mechanism for NO<sub>x</sub> in the presence of UHCs is shown in figure 5. The reactions of HO<sub>2</sub>, O<sub>3</sub> and  $\beta$ HAPs with NO produces NO<sub>2</sub>, OH and O<sub>2</sub>. Products



**Figure 5.** Reaction mechanism for NO<sub>x</sub> and  $C_3H_6$  chemistry. The key reaction is the conversion of NO to NO<sub>2</sub> by the  $\beta$ HAP radicals.

also include  $CH_3CH(OH)CH_2O$  and  $CH_3CH(O)CH_2OH$ ( $\beta$ -hydroxy alkoxy radicals, in short  $\beta$ HAs),

NO + CH<sub>3</sub>CH(OH)CH<sub>2</sub>OO 
$$\rightarrow$$
 NO<sub>2</sub> + CH<sub>3</sub>CH(OH)CH<sub>2</sub>O  
 $k = 2.7 \times 10^{-12} \exp\left(\frac{360}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k_{298} = 9.0 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  [36], (39)

NO + CH<sub>3</sub>CH(OO)CH<sub>2</sub>OH 
$$\rightarrow$$
 NO<sub>2</sub> + CH<sub>3</sub>CH(O)CH<sub>2</sub>OH  
 $k = 2.7 \times 10^{-12} \exp\left(\frac{360}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k = 9.0 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  [36], (40)

NO + HO<sub>2</sub> 
$$\rightarrow$$
 NO<sub>2</sub> + OH  
 $k = 3.5 \times 10^{-12} \exp\left(\frac{240}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k_{298} = 7.8 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  [36], (41)

NO + O<sub>3</sub> → NO<sub>2</sub> + O<sub>2</sub>  

$$k = 4.3 \times 10^{-12} \exp\left(-\frac{1598}{T}\right) \text{ cm}^3 \text{ s}^{-1},$$
  
 $k_{298} = 2.1 \times 10^{-14} \text{ cm}^3 \text{ s}^{-1}$  [36]. (42)

The time dependence of the densities of the  $\beta$ HAPs, HO<sub>2</sub> and O<sub>3</sub> for a single pulse and for the first and the last pulse of the high PRF case are shown in figure 6.  $\beta$ HAPs are produced by the reaction of O<sub>2</sub> with hydroxy alkyl radicals (produced by the reaction in equation (35)),

CH<sub>3</sub>CHCH<sub>2</sub>OH + O<sub>2</sub> → CH<sub>3</sub>CH(OO)CH<sub>2</sub>OH  

$$k = 1.2 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1}$$
 [36], (43)

CH<sub>3</sub>CH(OH)CH<sub>2</sub> + O<sub>2</sub> → CH<sub>3</sub>CH(OH)CH<sub>2</sub>OO  

$$k = 3.8 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$$
 [36], (44)

and are mainly consumed reactions with NO to form NO<sub>2</sub> and  $\beta$ HA radicals. Further reactions of  $\beta$ HA radicals then result in the formation of HCHO, CH<sub>3</sub>CHO and HO<sub>2</sub>,

CH<sub>3</sub>CH(OH)CH<sub>2</sub>O → CH<sub>3</sub>CHOH + HCHO  

$$k = 7.9 \times 10^{13} \exp\left(-\frac{10517}{T}\right) s^{-1},$$
  
 $k_{298} = 3.7 \times 10^{-2} s^{-1}$  [34], (45)

 $CH_3CHOH + O_2 \rightarrow CH_3CHO + HO_2$ 

$$k = 1.9 \times 10^{-11} \,\mathrm{cm}^3 \,\mathrm{s}^{-1}$$
 [39], (46)

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**Figure 6.** Time dependencies of the NO consuming radicals  $\beta$ HAPs, HO<sub>2</sub> and O<sub>3</sub>: (*a*) single pulse; (*b*) first of 20 repetitive pulses; (*c*) 20th of 20 pulses. Due to the depletion of NO with every pulse the residual radical densities increase with multiple pulses. O<sub>3</sub> being the least reactive of the three with NO has a larger residual density.

$$CH_3CH(O)CH_2OH \rightarrow CH_2OH + CH_3CHO$$
  

$$k = 9.1 \times 10^4 \,\mathrm{s}^{-1} \, [34], \qquad (47)$$

 $CH_2OH + O_2 \rightarrow HCHO + HO_2$ 

$$k = 2.0 \times 10^{-12} \,\mathrm{cm}^3 \,\mathrm{s}^{-1}$$
 [40]. (48)

The peak  $\beta$ HAP radical density during the first pulse of 20 pulses is  $\approx 2 \times 10^{13}$  cm<sup>-3</sup>. The decrease in this peak density during the 20th pulse (to  $1.5 \times 10^{13}$  cm<sup>-3</sup>) is primarily a result of the decrease in the density of C<sub>3</sub>H<sub>6</sub>, its precursor (discussed below).

The contributions of the reactions of  $O_2$  with CH<sub>3</sub>CHOH and CH<sub>2</sub>OH (equations (46) and (48)) to the formation of HO<sub>2</sub> when using multiple pulses are 27% and 50%, respectively. Other reactions which produce HO<sub>2</sub> include,

H + O<sub>2</sub> + M → HO<sub>2</sub> + M  

$$k = 1.8 \times 10^{-32} \left(\frac{T}{298}\right)^{-0.8} \text{ cm}^6 \text{ s}^{-1}$$
 [41], (49)

HCO + O<sub>2</sub> 
$$\rightarrow$$
 HO<sub>2</sub> + CO  
 $k = 2.0 \times 10^{-14} \left(\frac{T}{298}\right)^{2.4} \exp\left(\frac{768}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k_{298} = 2.6 \times 10^{-13} \text{ cm}^3 \text{ s}^{-1}$  [34], (50)



**Figure 7.** NO and NO<sub>2</sub> densities as a function of time for a single pulse with and without soot. With soot, the heterogeneous reaction of NO<sub>2</sub> regenerates NO in the gas phase. This reaction occurs on a timescale of  $\sim$ 10s of milliseconds when most of the NO consuming radicals are depleted. As a result, NO accumulates.

with their contributions being 2% (equation (49)) and 21% (equation (50)). With single pulses, the contributions to HO<sub>2</sub> production by O<sub>2</sub> reactions with CH<sub>3</sub>CHOH, CH<sub>2</sub>OH, H and HCO are 24%, 46%, 10% and 20%. The primary loss process for HO<sub>2</sub> radicals is the reaction with NO forming NO<sub>2</sub> and OH (equation (41)).

 $O_3$  is produced by the reaction of O with  $O_2$  (equation (34)) and is dominantly consumed by reaction with NO forming  $NO_2$ (equation (42)) and by reaction with  $O_2(^1\Delta)$  forming O,

$$\mathbf{e} + \mathbf{O}_2 \to \mathbf{O}_2(^1\Delta) + \mathbf{e},\tag{51}$$

$$O_{3} + O_{2}({}^{1}\Delta) \rightarrow O + O_{2} + O_{2}$$

$$k = 5.2 \times 10^{-11} \exp\left(-\frac{2840}{T}\right) \text{ cm}^{3} \text{ s}^{-1},$$

$$k_{298} = 3.8 \times 10^{-15} \text{ cm}^{3} \text{ s}^{-1} \text{ [39]}.$$
(52)

Due to the larger rate coefficients for reactions of NO with HO<sub>2</sub> and  $\beta$ HAP radicals compared to O<sub>3</sub>, HO<sub>2</sub> and  $\beta$ HAP radicals are more rapidly consumed than ozone. As a consequence, the O<sub>3</sub> density accumulates pulse to pulse, as shown in figure 6(*c*).

The densities of NO and NO<sub>2</sub> as a function of time with and without soot for a single pulse are shown in figure 7. Without soot NO is mainly consumed by reactions with  $\beta$ HAP radicals (34%), HO<sub>2</sub> (36%), CH<sub>3</sub>O<sub>2</sub> (3%) and C<sub>2</sub>H<sub>5</sub>O<sub>2</sub> (6%) to produce NO<sub>2</sub> by the reactions in equations (39)–(41). The reactions of NO with CH<sub>3</sub>O<sub>2</sub> and C<sub>2</sub>H<sub>5</sub>O<sub>2</sub> are

NO + CH<sub>3</sub>O<sub>2</sub> 
$$\rightarrow$$
 NO<sub>2</sub> + CH<sub>3</sub>O  
 $k = 4.2 \times 10^{-12} \exp\left(\frac{180}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k_{298} = 7.7 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  [39], (53)

NO + C<sub>2</sub>H<sub>5</sub>O<sub>2</sub> 
$$\rightarrow$$
 NO<sub>2</sub> + C<sub>2</sub>H<sub>5</sub>O  
 $k = 3.1 \times 10^{-12} \exp\left(\frac{330}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k_{298} = 9.4 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  [34]. (54)

 $CH_3O_2$  and  $C_2H_5O_2$  are formed by the reactions of  $CH_3$  and  $C_2H_5$  with  $O_2\colon$ 

CH<sub>3</sub> + O<sub>2</sub> + M → CH<sub>3</sub>O<sub>2</sub> + M  

$$k = 4.4 \times 10^{-31} \left(\frac{T}{298}\right)^{-3} \text{ cm}^{6} \text{ s}^{-1}$$
 [34], (55)

$$C_{2}H_{5} + O_{2} + M \rightarrow C_{2}H_{5}O_{2} + M$$

$$k = 8.0 \times 10^{-26} \left(\frac{T}{298}\right)^{-8.2} \exp\left(-\frac{2150}{T}\right) \text{ cm}^{6} \text{ s}^{-1},$$

$$k_{298} = 5.0 \times 10^{-29} \text{ cm}^{6} \text{ s}^{-1} \quad [42]. \quad (56)$$

 $CH_3$  and  $C_2H_5$  are produced by the reactions of O atoms with  $C_3H_6$  (equations (31) and (32)).

With soot particles,  $NO_2$  undergoes heterogeneous reactions on their surface to form NO and CO,

$$NO_{2(g)} \to NO_{2(ads)}, \qquad \gamma_0(NO_2) = 0.1 \ [27],$$
 (57)

$$NO_{2(ads)} \rightarrow NO_{(g)} + CO_{(g)}$$
  $k = 10^3 s^{-1}$  [26], (58)

resulting in an increase in the NO density at later times.

The time dependences of the densities of NO and NO<sub>2</sub> with and without soot for multiple pulses are shown in figure 8(*a*). Without soot, most of the NO is converted to NO<sub>2</sub> by reactions with  $\beta$ HAP radicals (42%), HO<sub>2</sub> (44%), O<sub>3</sub> (2%), CH<sub>3</sub>O<sub>2</sub> (5%) and C<sub>2</sub>H<sub>5</sub>O<sub>2</sub> (2%) (equations (39)–(42), (53) and (54)).



**Figure 8.** NO and NO<sub>2</sub> densities as a function of time for repetitive pulses with and without soot: (*a*) NO and NO<sub>2</sub> densities for all pulses; (*b*) NO density during the 12th pulse; (*c*) NO<sub>2</sub> density during the 12th pulse. The heterogeneous conversion of NO<sub>2</sub> on soot increases the gas phase density of NO and decreases the NO<sub>2</sub> density. After about 5 pulses, there are three distinct phases for NO evolution. Initial conversion of NO<sub>2</sub> to NO to NO<sub>2</sub> by reaction with O and N atoms, homogeneous conversion of NO to NO<sub>2</sub> by reaction with radicals such as  $\beta$ HAPs, HO<sub>2</sub> and O<sub>3</sub>, and heterogeneous generation of NO from NO<sub>2</sub>.

After the fifth pulse, the density of NO is less than that of NO<sub>2</sub>. Since radicals such as N, O, OH, HO<sub>2</sub> and CH<sub>3</sub>O are produced (equations (20)–(22), (49) and (53)) with every discharge pulse, the rate of reaction of these radicals with NO<sub>2</sub> increases relative to NO whose density decreases with each pulse. Without NO, the source of NO<sub>2</sub> removed and the density of NO<sub>2</sub> decreases with each pulse. The end products of the NO<sub>2</sub> conversion include NO (equations (26), (33)), HNO<sub>3</sub> (equation (37)), HNO<sub>2</sub> and CH<sub>3</sub>ONO<sub>2</sub>. HNO<sub>2</sub> is formed by the reaction of HO<sub>2</sub> with NO<sub>2</sub>,

HO<sub>2</sub> + NO<sub>2</sub> → HNO<sub>2</sub> + O<sub>2</sub>  

$$k = 1.2 \times 10^{-13} \text{ cm}^3 \text{ s}^{-1}$$
 [34]. (59)

CH<sub>3</sub>ONO<sub>2</sub> is formed by the reaction of CH<sub>3</sub>O with NO<sub>2</sub>,

CH<sub>3</sub>O + NO<sub>2</sub> → CH<sub>3</sub>ONO<sub>2</sub>  

$$k = 8.3 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$$
 [34]. (60)

With multiple pulses and soot, NO densities are generally higher and NO<sub>2</sub> densities are generally lower than without soot because of the heterogeneous conversion of NO<sub>2</sub> to NO on the soot surface. In any given pulse, there are three distinct phases for the evolution of the NO density as shown in figure 8(b) for the 12th pulse. In the first phase during the current pulse, there is a small and rapid production of NO from NO<sub>2</sub>. In the second phase following the current pulse and lasting approximately 3 ms, the NO density decreases primarily due to gas phase reactions with  $\beta$ HAP radicals and HO<sub>2</sub> (equations (39)–(41)), resulting in conversion to NO2. During the third phase, the NO density increases due to its heterogeneous production from the reaction of NO<sub>2</sub> with soot (equations (57) and (58)). For any given pulse, the gas phase consumption of NO is larger than its heterogeneous production, and so the NO density decreases. For pulses later than the fifth, the density of NO<sub>2</sub> is greater than NO. As a result, immediately following the current pulse, there is a rapid decrease in the density of NO2 and a corresponding increase in the NO density as shown in figures 8(b) and (c). This is due to the conversion of NO<sub>2</sub> to NO by reactions with O and N atoms (equations (26) and (33)) which are produced by electron impact reactions (equations (20) and (21)).

Since the density of NO decreases with every pulse, the rates of reaction of NO with  $\beta$ HAP radicals, O<sub>3</sub> and HO<sub>2</sub> decrease with each pulse. As a result, the rates of consumption of  $\beta$ HAP radicals, O<sub>3</sub> and HO<sub>2</sub> decrease with each pulse and so their densities at the end of a pulse increase with time. These trends are shown in figure 9.

In our previous work, we showed that the surface densities of O and OH on the soot are at least two orders of magnitude smaller than that of NO<sub>2</sub> and hence do not significantly influence the heterogeneous chemistry [14]. The time dependencies of the fraction of sites occupied by NO2 when using single and multiple pulses are shown in figure 10(a). With a single pulse, most of the adsorbed NO<sub>2</sub> desorbs to NO and CO. However, after a residence time of 0.2 s a significant fraction (15%) of the sites on the soot surface is still occupied by  $NO_2$ . When using multiple pulses, due to the smaller rate of production of NO<sub>2</sub> during any given pulse compared to a single pulse, a smaller fraction of the sites is occupied by NO<sub>2</sub>. However, due to the larger densities of NO2 at later times when using multiple pulses (see figure 8(a)), there is an increased flux of NO<sub>2</sub> to the soot. The end result is an increased rate of soot oxidation.



**Figure 9.** Densities of NO consuming radicals: (*a*)  $\beta$ HAPs; (*b*) O<sub>3</sub>; (*c*) HO<sub>2</sub>. Since the density of NO decreases with each pulse, the rate of reaction of NO with these radicals decreases. As a result, their residual densities increase with time.

The mass fractions of soot remaining as a function of time are shown in figure 10(b) for single and multiple pulses. The initial rates of oxidation are higher with single pulses because of the larger flux of NO<sub>2</sub> to the soot resulting from the initially larger NO<sub>2</sub> densities in the gas phase. At later times, there is a larger flux of NO<sub>2</sub> to the soot with multiple pulses (compare figures 7 and 8(*a*)) and, as a result, more soot oxidation occurs. This higher flux results from the conversion of NO to NO<sub>2</sub> by  $\beta$ HAP radicals and HO<sub>2</sub> (equations (39)–(41)). The diameters of the soot particles as a function of time for single and multiple pulses are shown in figure 10(c). As a result of oxidation, the diameter of the soot particles decreases to approximately 58 nm at the end of 0.2 s with a single pulse while with repetitive pulses, the exit soot diameter is 38 nm.

To investigate the consequences of complete desorption of NO<sub>2</sub> from the soot, the residence time of the gas was increased to 3 s while keeping the energy deposition and the number of pulses a constant. To maintain the 20 pulse format, the repetition rate was decreased to 7 Hz. With a single pulse almost all of the NO<sub>2</sub> desorbs from the surface as shown in figure 11(a). Due to the smaller production of NO<sub>2</sub> per pulse with multiple pulses, less NO<sub>2</sub> is adsorbed during the early pulses as shown in figure 11(b). However, due to the larger flux of NO<sub>2</sub> at later times, more soot is ultimately oxidized using multiple pulses. For example, the diameters of the soot



**Figure 10.** Surface properties of soot with single and multiple pulses as a function of time: (*a*) fraction of sites adsorbed with NO<sub>2</sub>; (*b*) soot mass fraction; (*c*) diameter of soot. After a few milliseconds, heterogeneous conversion of NO<sub>2</sub> on the soot regenerates NO with a single pulse. There is a constant flux of NO<sub>2</sub> to the soot using multiple pulses resulting in a larger adsorbed fraction. More soot oxidation also occurs.

as a function of time for the single and repetitive pulse cases (7 Hz) are shown in figure 11(*c*). With multiple pulses, the NO<sub>2</sub> densities are sustained for longer times and so almost complete soot oxidation occurs. With single pulses, most of the NO<sub>x</sub> for times >0.1 s is NO and so less soot oxidation occurs. The soot diameter decreases by only  $\approx$ 55% for the same energy deposition.

Soot leads to circular chemistry involving interconversion between NO and NO<sub>2</sub>, as shown in figure 12. In the absence of soot, the conversion of NO to NO<sub>2</sub> occurs by the reaction of NO with HO<sub>2</sub> which produces OH (equation (41)) and by the reactions of NO with  $\beta$ HAP radicals which lead to HO<sub>2</sub> formation (equations (39), (40) and (45)–(48)). The reaction of OH with C<sub>3</sub>H<sub>6</sub> starts a chain reaction resulting in the formation of  $\beta$ HAP radicals (equations (35), (43) and (44)). Thus, the reaction of HO<sub>2</sub> with NO leads to the formation of  $\beta$ HAP radicals and that of  $\beta$ HAPs with NO produces HO<sub>2</sub>. The products of the gas phase reactions converting NO to NO<sub>2</sub> are reactants for further NO to NO<sub>2</sub> conversion. With soot,



**Figure 11.** Soot properties for a residence time of  $3 ext{ s: } (a)$  site occupancy for a single pulse; (b) site occupancy for multiple pulses; (c) diameter of the soot. Almost all of the adsorbed NO<sub>2</sub> desorbs to produce NO with a single pulse. When using multiple pulses, the soot is almost completely oxidized due to the increased time for desorption between pulses.

heterogeneous conversion of NO<sub>2</sub> produces NO and as a result NO densities are sustained for longer periods of time. This leads to increased rates for the conversion of NO to NO<sub>2</sub> in the gas phase and a prolonged production of OH, HO<sub>2</sub> and  $\beta$ HAP radicals.

Due to the larger production of OH with soot more  $C_3H_6$ is consumed (equation (35)), as shown in figure 13(*a*). Soot does not significantly affect  $C_3H_6$  consumption using single pulses as the heterogeneous conversion of NO<sub>2</sub> to NO occurs on timescales > 1 ms by which time most of the radicals required for the conversion of NO to NO<sub>2</sub> have been consumed. As a result, the circular chemistry is less efficient. NO oxidizing radicals (e.g. HO<sub>2</sub>, O<sub>3</sub> and  $\beta$ HAP radicals) are produced during each pulse of the repetitive pulse case and so there is an increased overlap in time of the densities of NO and the oxidizing species. There is also a higher density of NO with soot. The combined effect of multiple pulses and soot is production of more OH (by the circular chemistry) which then results in increased consumption of  $C_3H_6$ , as shown in figures 13(*b*) and (*c*).



**Figure 12.** Circular NO and NO<sub>2</sub> chemistry. In the absence of soot particles, NO to NO<sub>2</sub> conversion by reaction with HO<sub>2</sub> produces OH, and by reactions with  $\beta$ HAPs leads to formation of HO<sub>2</sub>. The reaction of OH with C<sub>3</sub>H<sub>6</sub> starts a chain reaction which results in the formation of  $\beta$ HAPs. The reaction of HO<sub>2</sub> with NO therefore leads to the formation of  $\beta$ HAPs and those of  $\beta$ HAPs with NO lead to HO<sub>2</sub> formation. The products of the conversion of NO to NO<sub>2</sub> are themselves the reactions for further NO to NO<sub>2</sub> conversion. With soot, this cycle is more pronounced due to the heterogeneous conversion of NO<sub>2</sub> back to NO.



**Figure 13.** Molecular and radical densities for cases with and without soot as a function of time: (*a*)  $C_3H_6$  for a single pulse; (*b*)  $C_3H_6$  for multiple pulses; (*c*) OH for 20th of 20 pulses. Due to the more pronounced circular chemistry with soot, more OH production results and so more  $C_3H_6$  is consumed. There is increased overlap in time of reacting species densities with multiple pulses and so larger  $C_3H_6$  consumption occurs.

In order to track the large dynamic ranges in densities of radicals over large dynamic ranges in time, the densities have to this point to be expressed in cm<sup>-3</sup>. However, it is typical for measures of remediation to be expressed in ppmv (parts per million by volume) or simply ppm for comparison with the emission standards expressed in such units. These units will be used in the following discussion. For the operating conditions of interest (1 atm, 453 K), 1 ppm =  $1.62 \times 10^{13}$  cm<sup>-3</sup> (initial NO density = 260 ppm =  $4.2 \times 10^{15}$  cm<sup>-3</sup>).

Increasing energy deposition with single pulses results in increased NO conversion, as shown in figure 14(a). (Energy deposition was varied by changing the applied voltage.) At  $60J1^{-1}$ , NO densities decrease to approximately 125 ppm resulting in an NO conversion of 52%. This higher rate of NO consumption at larger energy deposition is primarily due to the chain chemistry producing N<sub>2</sub> and HNO<sub>2</sub> by the reactions in equations (24) and (38). At higher energy deposition, there is also an increased production of O atoms which generates more CH<sub>3</sub> and C<sub>2</sub>H<sub>5</sub> by reactions with C<sub>3</sub>H<sub>6</sub> (equations (31) and (32)). This results in increased formation of CH<sub>3</sub>O and



**Figure 14.** Remediation parameters as a function of energy deposition: (*a*) gas phase densities of NO and NO<sub>2</sub>, and fraction of surface sites on soot adsorbed with NO<sub>2</sub> for a single pulse; (*b*) gas phase densities of NO and NO<sub>2</sub>, and fraction of surface sites on soot adsorbed with NO<sub>2</sub> with multiple pulses; (*c*) *W*-value for NO<sub>x</sub> for single and multiple pulses. Multiple pulses are more efficient for NO<sub>x</sub> removal due to the increased overlap in time of densities of NO<sub>2</sub> and NO with consuming radical densities.

C<sub>2</sub>H<sub>5</sub>O (equations (53) and (54)), which then consume NO by CH<sub>3</sub>O + NO  $\rightarrow$  CH<sub>3</sub>ONO

$$k = 2.0 \times 10^{-11} \,\mathrm{cm}^3 \,\mathrm{s}^{-1}$$
 [34], (61)

C<sub>2</sub>H<sub>5</sub>O + NO → C<sub>2</sub>H<sub>5</sub>ONO  

$$k = 2.0 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1}$$
 [34]. (62)

The exit composition of  $NO_x$  is primarily NO because of the heterogeneous conversion of  $NO_2$  to NO on the soot (equations (57) and (58)). The fraction of sites on the soot occupied by  $NO_2$  is maximum at approximately 0.15 when the  $NO_2$  density peaks and subsequently decreases as the  $NO_2$ flux decreases at higher energy deposition. This decrease in  $NO_2$  density is largely a result of reactions with radicals such as OH, CH<sub>3</sub>O, C<sub>2</sub>H<sub>5</sub>O<sub>2</sub> and HO<sub>2</sub> to produce HNO<sub>3</sub>, HNO<sub>2</sub>, CH<sub>3</sub>ONO<sub>2</sub> (equations (37), (59) and (60)). C<sub>2</sub>H<sub>5</sub>OONO<sub>2</sub> is also produced by

$$C_{2}H_{5}O_{2} + NO_{2} \rightarrow C_{2}H_{5}OONO_{2}$$

$$k = 2.6 \times 10^{-10} \left(\frac{T}{298}\right)^{-3.7} \exp\left(-\frac{1029}{T}\right) \text{ cm}^{3} \text{ s}^{-1},$$

$$k_{298} = 8.2 \times 10^{-12} \text{ cm}^{3} \text{ s}^{-1} \text{ [34]}.$$
(63)

With increasing energy deposition with repetitive pulses, HO<sub>2</sub>, O<sub>3</sub> and  $\beta$ HAP radicals are produced on every pulse and so the heterogeneously generated NO is more effectively converted to NO<sub>2</sub>. As a result, NO densities decrease more rapidly with energy deposition, as shown in figure 14(*b*). The reactions responsible for the decrease in the NO<sub>2</sub> density with energy deposition are similar to those for a single pulse, however the decrease is more pronounced because of the increased overlap in time of NO<sub>2</sub> and OH, CH<sub>3</sub>O, C<sub>2</sub>H<sub>5</sub>O<sub>2</sub> and HO<sub>2</sub> densities following each pulse. The fraction of sites occupied by adsorbed NO<sub>2</sub> is in general larger with multiple pulses due to the larger NO<sub>2</sub> density.

The W-values for  $NO_x$  with single and multiple pulses are shown in figure 14(c). In general repetitive pulses are more efficient (lower W-value) compared to single pulses. At the base case energy of  $30 \text{ J} \text{ I}^{-1}$ , the W-value for NO<sub>x</sub> for a single pulse is 152 eV and for multiple pulses is 120 eV. The increase in efficiency is primarily a result of increased conversion of NO<sub>2</sub> to HNO<sub>3</sub>, CH<sub>3</sub>ONO<sub>2</sub>, C<sub>2</sub>H<sub>5</sub>OONO<sub>2</sub> and HNO<sub>2</sub>. The densities of these nitrogen containing products, shown in figure 15, are higher for multiple pulses as a result of the increased overlap in time of the densities of NO<sub>2</sub> and the participating radical species (e.g. OH, CH<sub>3</sub>O, C<sub>2</sub>H<sub>5</sub>O<sub>2</sub> and  $HO_2$ ). At 60 J1<sup>-1</sup>, approximately 70 ppm of HNO<sub>2</sub> are produced using repetitive pulses whereas only 35 ppm are formed using single pulses. At the same energy deposition, repetitive multiple pulses produce approximately 40 ppm of organic nitrates (C<sub>2</sub>H<sub>5</sub>OONO<sub>2</sub> and CH<sub>3</sub>ONO<sub>2</sub>) while with single pulses only 10 ppm are produced.

Important hydrocarbon products of  $C_3H_6$  dissociation include aldehydes such as HCHO and CH<sub>3</sub>CHO. The exit densities of HCHO and CH<sub>3</sub>CHO as a function of energy deposition are shown in figure 15(*c*). HCHO and CH<sub>3</sub>CHO are produced from the reactions of the  $\beta$ HA radicals (equations (45)–(48)). More  $C_3H_6$  is consumed (see figure 12) with repetitive pulses leading to an increased production of  $\beta$ HAP radicals (equations (35), (43) and (44)). This results in





**Figure 15.** Densities of nitrogen containing products and aldehydes as a function of time when using single and multiple pulses with soot: (*a*) HNO<sub>3</sub> and HNO<sub>2</sub>; (*b*) CH<sub>3</sub>ONO<sub>2</sub> and C<sub>2</sub>H<sub>5</sub>OONO<sub>2</sub>; (*c*) CH<sub>3</sub>CHO and HCHO. Due to the increased overlap in time of the densities of NO and NO<sub>2</sub> with the radicals produced during each pulse, multiple pulses in general lead to larger densities of aldehydes and nitrogen containing products.

increased formation of  $\beta$ HA radicals (equations (39) and (40)) which are the precursors to HCHO and CH<sub>3</sub>CHO production (equations (45)–(48)). The HCHO density decreases at higher energy depositions owing to consumption by reaction with OH (equation (36)).

The mass fractions of soot remaining as a function of energy deposition for single and repetitive pulses are shown in figure 16(*a*). At energy depositions  $>20 \text{ JI}^{-1}$ , the NO<sub>2</sub> density in the gas phase for single pulses decreases because of increased NO<sub>2</sub> consumption by the reactions in equations (37), (59), (60) and (63). As a result, a smaller amount of soot is

**Figure 16.** Soot removal parameters as a function of energy deposition when using single and multiple pulses: (*a*) mass fraction of soot; (*b*) *W*-value for soot oxidation; (*c*) increase in CO. In general multiple pulses are more efficient for soot oxidation because of the sustained densities of NO<sub>2</sub> compared to the single pulse case.

oxidized at higher energies. The larger NO<sub>2</sub> densities obtained with increasing energy deposition with repetitive pulses result in higher rates of adsorption on the soot. Consequently, more soot is oxidized. The *W*-values for soot removal (J  $\mu$ g<sup>-1</sup>) are shown as a function of energy deposition in figure 16(*b*). Using multiples pulse in general results in more efficient soot removal due to the sustained densities of NO<sub>2</sub> which oxidize the soot. The *W*-value for soot at 30 J1<sup>-1</sup> is about 0.3 J  $\mu$ g<sup>-1</sup> for multiple pulses and 0.5 J  $\mu$ g<sup>-1</sup> for single pulses.

CO is an end product not only of soot oxidation (equation (58)) but also of gas phase reactions such as the electron impact dissociation of  $CO_2$  (equation (23)) and the

reaction of HCO with O<sub>2</sub>,  
HCO + O<sub>2</sub> 
$$\rightarrow$$
 CO + HO<sub>2</sub>  
 $k = 2.0 \times 10^{-14} \left(\frac{T}{298}\right)^{2.4} \exp\left(\frac{768}{T}\right) \text{ cm}^3 \text{ s}^{-1},$   
 $k = 2.6 \times 10^{-13} \text{ cm}^3 \text{ s}^{-1}$  [34]. (64)

HCO is formed by the reactions of O with  $C_3H_6$  (equation (32)) and OH with HCHO (equation (36)). CO exit densities as a function of energy deposition are shown in figure 16(*c*). Increasing energy deposition leads to increased rates of CO<sub>2</sub> dissociation and HCO formation (due to higher O and OH production) resulting in higher CO densities. Larger densities of HCO are generated with repetitive pulses due to the larger production of OH. These larger densities also result in increased CO formation (equation (64)).

Due to the variations in the composition of diesel fuel and the combustion parameters, the UHC concentration in the exhaust can fluctuate. To this end, we investigated the sensitivity of NO<sub>x</sub> removal to the inlet UHC concentration when using multiple pulses. All other conditions are the same as the base case. The removal of NO<sub>x</sub> improves with increasing  $C_3H_6$ , as shown in figure 17. This trend is a result of increased nitrate and HNO<sub>x</sub> formation by the reactions in equations (37) and (59)–(63). For example, the increasing densities of HNO<sub>2</sub> with increasing  $C_3H_6$  are also shown in figure 17. Increased production of OH and HO<sub>2</sub> occur with soot by increased cyclic conversion between NO and NO<sub>2</sub> resulting in larger rates of HNO<sub>2</sub> formation (equations (38) and (59)).

The effects of soot particle number density and diameter on NO<sub>x</sub> remediation were investigated. Increasing either the diameter of the soot or its number density results in increased exit densities of NO when using single pulses, as shown in figure 18(*a*). The increase in NO is a result of the heterogeneous conversion of NO<sub>2</sub> to NO following the larger surface area of the soot. At small soot diameters and soot densities (40 nm,  $10^7 \text{ cm}^{-3}$ ), negligible heterogeneous conversion of NO<sub>2</sub> to NO occurs and so most of the NO<sub>2</sub> produced in the gas phase exits the reactor. At large soot diameters and soot densities (200 nm,  $10^9 \text{ cm}^{-3}$ ) most of



**Figure 17.** NO<sub>x</sub> and HNO<sub>2</sub> densities as a function of  $C_3H_6$  inlet density for multiple pulses. There is increased NO<sub>2</sub> to NO conversion with soot and so larger NO and HNO<sub>3</sub> densities result. The interconversion between NO and NO<sub>2</sub> is a combined result of the heterogeneous reaction of NO<sub>2</sub> and the homogeneous conversion of NO by  $\beta$ HAP radicals. With increasing densities of UHCs, larger densities of  $\beta$ HAPs are generated and the rate of interconversion between NO and NO<sub>2</sub> increases, leading to the increased formation of HNO<sub>2</sub>, and larger NO<sub>x</sub> removal.

the NO<sub>2</sub> is converted to NO by heterogeneous reactions. Heterogeneous reactions occur on a timescale of ~10s of milliseconds at which time most of the radicals which convert NO to NO<sub>2</sub> (e.g.  $\beta$ HAPs, HO<sub>2</sub> and O<sub>3</sub>) have been consumed. As a result, the exit composition of NO<sub>x</sub> is primarily NO. Since the heterogeneous NO<sub>x</sub> reactions result in only the conversion of NO<sub>2</sub> to NO, the total NO<sub>x</sub> density remains nearly a constant, as shown in figure 18(*b*).

The densities of NO and  $NO_x$  as a function of soot density and diameter for repetitive pulses are shown in figure 19. The production of NO consuming radicals during each pulse (see figure 9) results in the gas phase conversion of NO to NO<sub>2</sub>. As a result the NO densities are smaller compared to using a single pulse. At either small soot densities and large diameters, or at large soot densities and small diameters, the homogeneous conversion of NO to NO<sub>2</sub> dominates the heterogeneous conversion of NO2 to NO and so most of the  $NO_x$  is  $NO_2$ . However, at large soot densities and large diameters  $(10^9 \text{ cm}^{-3}, 200 \text{ nm})$ , the rates for the heterogeneous conversion of NO2 to NO exceed the rates for the homogeneous conversion of NO to NO<sub>2</sub> and so the exit composition of  $NO_x$  is dominantly NO. The homogeneous and heterogeneous processes involving NO and NO<sub>2</sub> result mainly in their interconversion and so the total NO<sub>x</sub> density almost remains unaffected. The smaller  $NO_x$  density with multiple pulses is due to the increased rates of reactions of NO and NO<sub>2</sub>



**Figure 18.** NO and NO<sub>x</sub> exit densities as a function of soot density and diameter when using a single pulse: (*a*) NO; (*b*) NO<sub>x</sub>. Increasing the soot density and diameter results in a larger surface area for heterogeneous NO<sub>2</sub> to NO conversion leading to larger exit densities of NO. Since this process only converts NO<sub>2</sub> to NO, the overall NO<sub>x</sub> density remains nearly a constant.



**Figure 19.** NO and NO<sub>x</sub> exit densities as a function of soot density and diameter when using multiple pulses: (*a*) NO; (*b*) NO<sub>x</sub>. Due to the increased overlap in time of radical densities and the densities of NO and NO<sub>2</sub>, more NO<sub>x</sub> removal occurs compared to using single pulses. The interconversion between NO and NO<sub>2</sub> only leads to a change in the composition of NO<sub>x</sub> without appreciably altering its density.

with radicals such as CH<sub>3</sub>O (equations (60) and (61)),  $C_2H_5O$  (equation (62)),  $C_2H_5O_2$  (equation (63)), OH (equations (37) and (38)) and HO<sub>2</sub> (equation (59)), producing CH<sub>3</sub>ONO<sub>2</sub>, CH<sub>3</sub>ONO,  $C_2H_5ONO$ ,  $C_2H_5ONO_2$ , HNO<sub>2</sub> and HNO<sub>3</sub>. The increased rates are a result of the increased overlap in time of the densities of NO and NO<sub>2</sub> with the radical densities.

## 4. Concluding remarks

The effects of repetitive pulses and soot chemistry on the plasma remediation of  $NO_x$  using DBDs were investigated. In the absence of soot, using repetitive pulses resulted in higher conversion of NO to NO<sub>2</sub> compared to using a single pulse case. Single pulses with soot result in an initial gas phase oxidation of NO to NO<sub>2</sub>, followed by a heterogeneous conversion of NO<sub>2</sub> to NO on the soot. Due to the larger gas phase NO<sub>2</sub> density using repetitive pulses, there is an increased flux of NO2 to the soot surface, resulting in increased soot oxidation and larger rates of heterogeneous conversion of NO<sub>2</sub> to NO. At 30 J l<sup>-1</sup>, using single pulses with and without soot produced about 30% NO<sub>x</sub> removal. The final NO<sub>x</sub> was primarily NO<sub>2</sub> (almost 100%) in the absence of soot whereas with soot the NO<sub>x</sub> was 88% NO and 12% NO<sub>2</sub>. When using multiple pulses,  $30 \text{ J} \text{ I}^{-1}$  resulted in 35% NO<sub>x</sub> removal in the absence of soot and 37% with soot. The W-value for soot oxidation at  $30 \text{ J} \text{ I}^{-1}$  improved from  $0.5 \text{ J} \mu \text{g}^{-1}$  with a single pulse to  $0.3 \text{ J} \mu \text{g}^{-1}$  with multiple pulses. The combined effects of multiple pulses and heterogeneous chemistry on NO<sub>x</sub> remediation and soot oxidation are two-fold. Improved NO<sub>x</sub> removal by the increased production of HNO<sub>2</sub>, HNO<sub>3</sub>, organic nitrates and nitrites due to the more favourable overlap in time of NO<sub>2</sub> and reactive radical densities; and increased soot oxidation because of larger NO<sub>2</sub> densities.

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### References

- Sun W, Pashaie B, Dhali S and Honea F 1996 J. Appl. Phys. 79 3438
- [2] Niessen W, Wolf O, Schruft R and Neiger M 1998 J. Phys. D: Appl. Phys. 31 542
- [3] Mok Y S and Nam I 1999 Trans. Plasma Sci. 27 1188
- [4] Park J Y, Toicic I, Round F G and Chang J S 1999 J. Phys. D: Appl. Phys. 32 1006
- [5] Rozoy M, Postel C and Puech V 1999 Plasma Sources Sci. Technol. 8 337
- [6] Takaki K, Jani M A and Fujiwara T 1999 Trans. Plasma Sci. 27 1137
- [7] Filimonova E A, Amirov R H, Kim H T and Park I H 2000 J. Phys. D: Appl. Phys. 33 1716
- [8] Dorai R and Kushner M J 2000 J. Appl. Phys. 88 3739
- [9] Penetrante B M, Brusasco R M, Merritt B T, Pitz W J, Vogtlin G E, Kung M C, Kung H H, Wan C Z and Voss K E 1998 SAE Technical Paper Series 982508
- [10] Hoard J and Balmer M L 1998 SAE Technical Paper Series 982429
- [11] Balmer M L, Tonkyn R, Yoon S, Kolwaite A, Barlow S, Maupin G, Orlando T and Hoard J 1999 SAE Technical Paper Series 1999-01-3640
- [12] Lary D J, Lee A M, Toumi R, Newchurch M J, Pirre M and Renard J B 1997 J. Geophys. Res. 102 3671
- [13] Thomas S E, Martin A R, Raybone D, Shawcross J T, Ng K L, Beech P and Whitehead J C 2000 SAE Technical Paper Series 2000-01-1926
- [14] Dorai R, Hassouni K and Kushner M J 2000 J. Appl. Phys. 88 6060
- [15] Penetrante B M, Hsiao M C, Merritt B T, Vogtlin G E, Wallman P H, Neiger M, Wolf O, Hammer T and Broer S 1996 Appl. Phys. Lett. 68 3719
- [16] Deryugin A, Napartovich A, Gorse C, Paniccia F and Capitelli M 1997 Plasma Chem. Plasma Process. 17 79
- [17] Wegst R, Neiger M, Russ H and Liu S 1999 SAE Technical Paper Series 1999-01-3686
- [18] Müller S, Conrads J and Best W 2000 Proc. Int. Symp. on High Pressure, Low Temperature Plasma Chemistry (Germany: Griefswald) vol 2, p 340
- [19] Müller S 2001 Proc. XXV Int. Conf. on Phenomena in Ionized Gases (Japan: Nagoya) vol 4, p 99
- [20] Finlayson-Pitts B J and Pitts J N 1994 Atmospheric Chemistry: Fundamentals and Experimental Techniques (New York: Wiley)
- [21] Dorai R and Kushner M J 2001 J. Phys. D: Appl. Phys. 34 574
- [22] Rockwood S D 1973 Phys. Rev. A 8 2348
- [23] Brown P N, Hindmarsh A and Byrne G D 1998 VODE—Variable-coefficient Ordinary Differential Equation solver
- [24] Neeft J P A, Makkee M and Moulijn J A 1996 Fuel Process. Technol. 47 1

- [25] Mitchell P and Frenklach M 1998 Proc. 27th Int. Symp. on Combustion (Pittsburgh, PA: The Combustion Institute) pp 1507–14
- [26] Tabor K, Gutzwiller L and Rossi M J 1994 J. Phys. Chem. 98 6172
- [27] Rogaski C A, Golden D M and Williams L R 1997 Geophys. Res. Lett. 24 381
- [28] Ngo T, Sander E J, Tong W M, Williams R S and Anderson M S 1994 *Surf. Sci.* **314** L817
- [29] Harano A, Sadakata M and Sato M 1991 J. Chem. Eng. Japan 24 100
- [30] Akhter M S, Chughtai A R and Smith D M 1984 J. Phys. Chem. 88 5334
- [31] Hoard J, Laing P, Balmer M L and Tonkyn R 2000 SAE Technical Paper Series 2000-01-2895
- [32] Ikezoe Y, Matsuoka S, Takebe M and Viggiano A 1987 Gas Phase Ion-Molecule Reaction Rate Constants Through

1986 (Tokyo: Ion Reaction Research Group of The Mass Spectroscopy Society of Japan)

- [33] Person J C and Ham D O 1988 Radiat. Phys. Chem. 31 1
- [34] Mirokin Y and Mallard G 1998 The NIST Chemical Kinetics Database
- [35] Atkinson R, Baulch D L, Cox R A, Hampson R F Jr, Kerr J A and Troe J 1989 J. Phys. Chem. Ref. Data 18 881
- [36] Atkinson R 1997 J. Phys. Chem. Ref. Data 26 215
- [37] Baulch D L 1992 J. Phys. Chem. Ref. Data 21 411
- [38] Tsang W and Herron J T 1991 J. Phys. Chem. Ref. Data 20 609
  [39] Atkinson R, Baulch D L, Cox R A, Hampson R F Jr, Kerr J A,
- Rossi M J and Troe J 1997 J. Phys. Chem. Ref. Data 26 521
- [40] Tsang W 1987 J. Phys. Chem. Ref. Data 16 471
- [41] Baulch D L et al 1994 J. Phys. Chem. Ref. Data 23 847
   [42] Wagner A F, Slagle I R, Sarzynski D and Gutman D 1990 J. Phys. Chem. 94 1853